

Engineering Bulletin
Puromet™
MTS9300
Macroporous
Iminodiacetic
Chelating Resin

For the selective removal of heavy
metals from aqueous solutions.



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Purolite is a leading manufacturer of ion exchange, catalyst, adsorbent and specialty resins. With global headquarters in the United States of America, Purolite focuses 100% of its resources on the development and production of resin technology.

Responding to our customers' needs, Purolite has a wide variety of products and the industry's largest technical sales force. Globally, we have strategically located research and development centers and application laboratories. Our ISO 9001 certified manufacturing facilities in the USA, United Kingdom, Romania and China combined with more than 40 sales offices in 30 countries ensure complete worldwide coverage.

Purolite has been part of Ecolab since 2021. A trusted partner at nearly three million commercial customer locations, Ecolab (ECL) is the global leader in water, hygiene and infection prevention solutions and services. Ecolab delivers comprehensive solutions, data-driven insights and personalized service to advance food safety, maintain clean and safe environments, optimize water and energy use, and improve operational efficiencies and sustainability for customers in the food, healthcare, hospitality and industrial markets in more than 170 countries around the world.



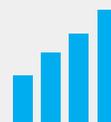
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The quality and consistency of our products is fundamental to our performance. Throughout all Purolite plants, production is carefully controlled to ensure that our products meet the most stringent criteria, regardless of where they are produced.



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Our continued investment in research and development means we are always perfecting and discovering innovative uses for ion exchange resins and adsorbents. We strive to make the impossible possible.

Engineering Bulletin: Puromet MTS9300 Macroporous Iminodiacetic Chelating Resin

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Product Description

Puromet MTS9300 is a macroporous polystyrene based chelating resin, with iminodiacetic groups designed for the removal of heavy metal cations from industrial effluents. These cations may be separated from high concentrations of monovalent cations (typically sodium) and also from common divalent cations (such as calcium). Removal can be achieved both from weakly acidic and weakly basic solutions depending on the metals to be removed. Puromet MTS9300 finds use in processes for extraction and recovery of metals from ores, galvanic plating solutions, pickling baths and effluents even in the presence of alkaline earth metals (calcium and magnesium).

Further important uses include refining salt solutions of transition and precious metals and for the cleaning and purification of various organic or inorganic chemical products by removal of heavy metals contamination (usually from aqueous solutions).

TABLE 1 Typical Physical and Chemical Characteristics

Characteristics	Description/Value
Polymer Structure	Macroporous polystyrene crosslinked with divinylbenzene
Appearance	Spherical beads
Functional Group	Iminodiacetic
Ionic Form	Na ⁺ form
Copper Capacity (min.)	50 g/L
Moisture Retention	52–60% (Na ⁺ form)
Particle Size Range	425–1000 μm
< 425 μm (max.)	2%
Uniformity Coefficient (max.)	1.5
Reversible Swelling, H ⁺ → Na ⁺ (max.)	35%
Specific Gravity	1.18
Shipping Weight (approx.)	750–800 g/L (46.9–50.0 lb/ft ³)
Temperature Limit	80 °C (176.0 °F)

Standard Operating Conditions

These operating conditions are given as a general example. However, regeneration conditions and flow rates should be chosen for the particular application. For further recommendations, please contact your local Purolite sales office.

TABLE 2 Standard Operating Conditions

Operation	Rate	Solution	Minutes	Amount
Service	8–16 BV/h 1–2 gpm/ft ³	For Treatment	–	–
Backwash	5–7 BV/h 2–3 gpm/ft ³	Raw Water	10–20	1.5–6 BV 10–35 gal/ft ³
Regeneration	3–4 BV/h 0.4–0.5 gpm/ft ³	6–10% HCl 6–10% H ₂ SO ₄ *	30–60	140–200 g/L HCL or 12.5–20 lb/ft ³ 200–320 g/L H ₂ SO ₄
Slow Rinse	3–4 BV/h 0.4–0.5 gpm/ft ³	Raw Water	30–40	2–3 BV 15–25 gal/ft ³
Conversion to sodium form as required	3–4 BV/h 0.4–0.5 gpm/ft ³	2–4% NaOH (Upflow)**	30–60	40–100 g/L 2.5–6.25 lb/ft ³
Rinse	3–4 BV/h 0.4–0.5 gpm/ft ³	Soft or Demin Water	20–40	2–4 BV 15–30 gal/ft ³

Backwash expansion 75% (optimum)
Design rising space 80–100%
Minimum bed depth 1,000 mm
"Gallons" refer to U.S. Gallon = 3.785 liters

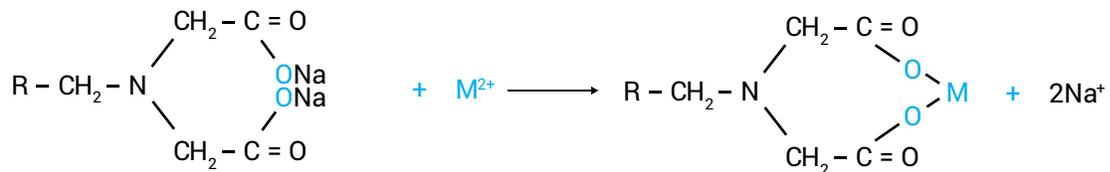
* The use of H₂SO₄ should be avoided, where Puromet MTS9300 is operated on feed solutions, which contain Ca. This is to avoid CaSO₄ precipitations.

** The aim is to achieve the same pH as that of the incoming solution.

For better performance, two columns can be operated in series with a third on stand-by to achieve lowest leakage.

Principle of Reaction

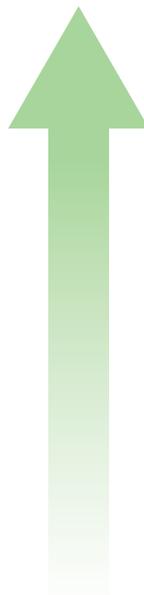
The iminodiacetic functional groups, in either the sodium or the hydrogen form, will chelate heavy metals by ion attraction to the dicarboxylic functionality and electron donation from the nitrogen:



Applications

FIGURE 1

**Selectivity
of Puromet
MTS9300 in
Acidic to Neutral
Conditions**



Iron (Ferric)
Copper
Hydrogen
Lead
Nickel
Cadmium
Zinc
Cobalt
Iron (Ferrous)/Manganese
Calcium/Magnesium
Strontium
Sodium

Puromet MTS9300 is particularly suitable for the removal of heavy metals (as weakly acidic chelated complexes). Relative selectivity of Puromet MTS9300 in acid to neutral conditions as shown in Figure 1:

$\text{Fe}^{3+} > \text{Cu} > \text{H} > \text{Pb} > \text{Ni} > \text{Cd} > \text{Zn} > \text{Co} > \text{Fe}^{2+} > \text{Mn} > \text{Mg} > \text{Ca} > \text{Sr} \gg \text{Na}^+$

The macroporous resin structure ensures excellent diffusion of ions thus affording efficient exhaustion and regeneration. Recovery of heavy metals from effluents from the plating industry is achieved by concentration and is particularly useful where full demineralization and recycling of the rinse water is not practiced. The simplest case is where only one heavy metal is present, when volumes of rinse water are low, wastewater fees may be low and raw water has a low salt content. Puromet MTS9300 can be used to reduce residual toxic heavy metals to below the maximum admissible concentration levels which are often far below those obtainable after precipitation reactions. It may also be used to remove similar residuals from demineralized rinse water circuits.

Puromet MTS9300 is also used to separate and concentrate heavy metals in hydro-metallurgical processes (ore dressing and scrap recovery). It is particularly suitable where metals are present in low concentrations. Separation techniques may be carried out according to the order of selectivity given above. However, changes in the sequence occur with change in pH and in the presence of certain anions (including higher concentrations of chloride and sulfate). The sequence given above is applicable for neutral and weakly acidic solutions. The optimal pH for this resin is 5–6 for greatest capacity but will work between a pH of 4–8. When the pH is greater than 9, the resin becomes more selective for calcium and magnesium which will use up capacity very quickly.

Operating Performance

The information below may be taken as a general guide. However, before any plant design is contemplated, the user should perform column testing of the feed solution to be treated.

The operating capacity is a function of pH and inlet concentration for each metal. Figures 2 and 3 provide estimated resin capacity for each metal based on pH. Actual loading will best be determined by piloting and testing during the service cycle.

FIGURE 2

Exchange Capacity for Metals as a Function of pH

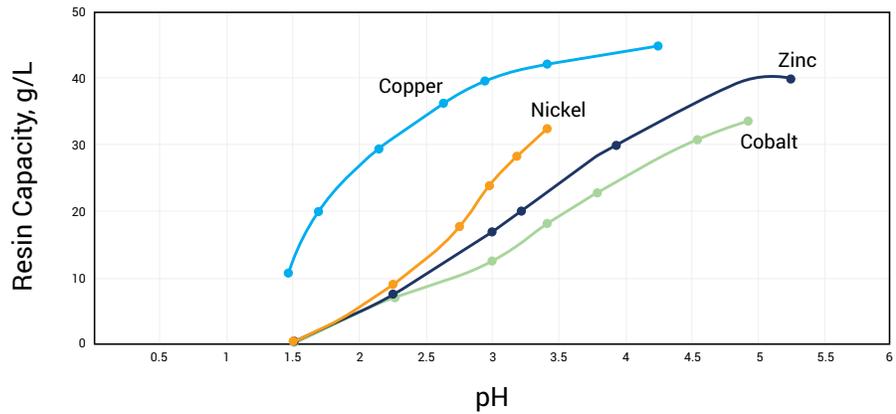
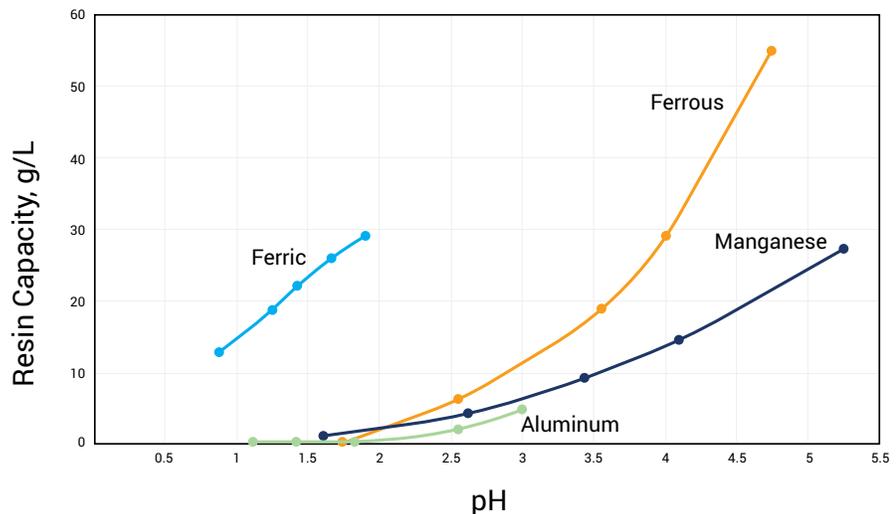


FIGURE 3

Exchange Capacity for Metals as a Function of pH



Hydraulic Characteristics (General Applications)

The pressure drop (or head loss) across a properly classified bed of ion-exchange resin depends on the particle size distribution, bed depth, flow rate, viscosity, and temperature of the influent solution. Anything affecting any of these parameters – for example, the presence of particulate matter filtered out by the bed, abnormal compaction of the resin bed, or the incomplete classification of the bed – will have an adverse effect and result in an increased head loss or pressure drop. Service flow rates from 8–16 bed volumes per hour, 1–2 gpm/ft³, depending on the application, may be regarded as the normal range used with this resin.

Pressure drop values expected for aqueous solutions, are given in Figure 4. This is applicable to the freshly regenerated H⁺ form. As the resin is converted to the metal form, the pressure drop will decrease slightly due to swelling during exhaustion from the H⁺ form.

During upflow backwash, the resin bed should be expanded by between 50 and 75%, to free any particulate matter, to clear the bed of entrapped air bubbles, and to reclassify the resin particles as much as possible, ensuring minimum resistance to flow. Bed expansion increases with backwash flow rate and decreases with temperature, as shown in Figure 5, for a typical exhausted form of the resin. Care should always be taken to avoid resin loss by over expansion of the bed.

FIGURE 4
**Pressure Drop vs
Flowrate**

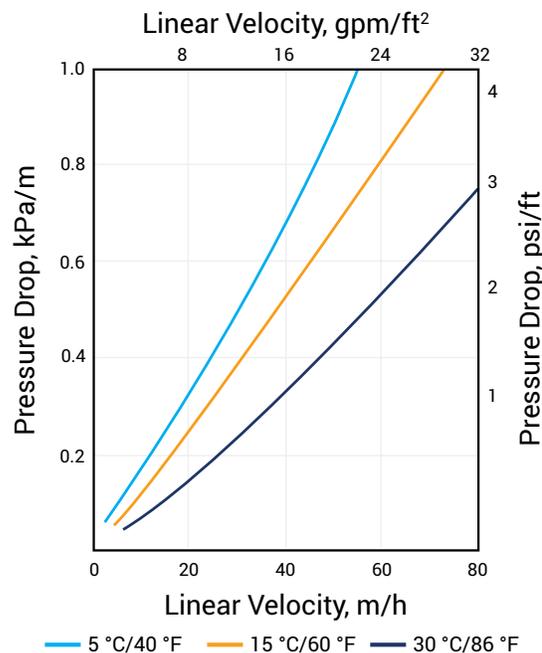


FIGURE 5

**Backwash Expansion
(Exhausted Form)**

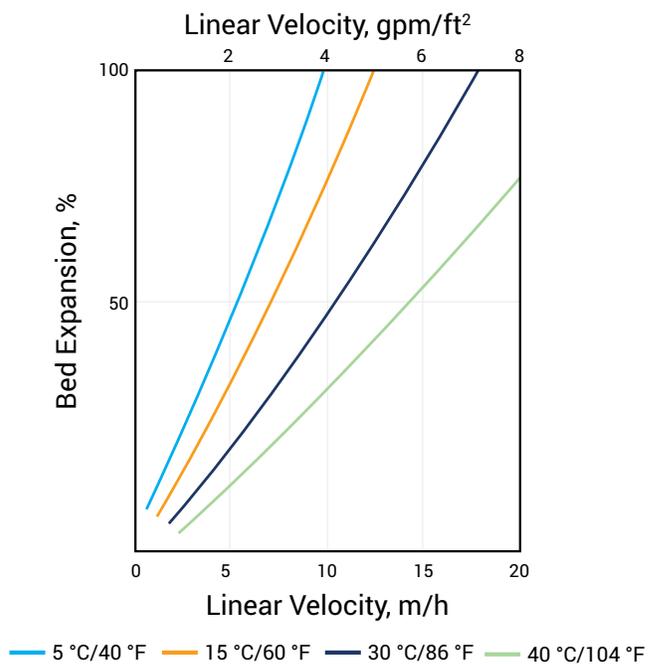


TABLE 5 Conversion of Units

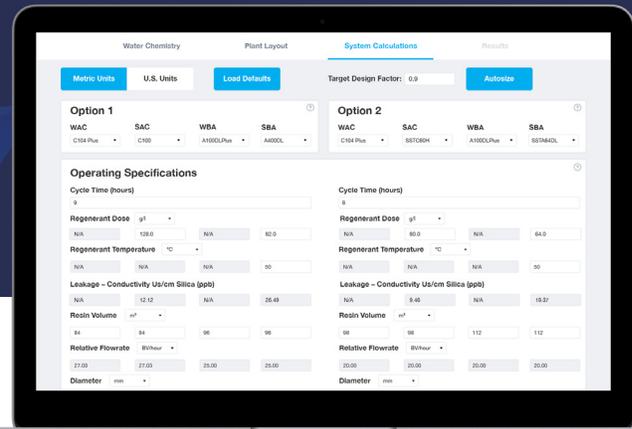
1 m/h (Cubic Meters Per Square Meter Per Hour)	= 0.341 gpm/ft ² = 0.409 U.S. gpm/ft ²
1 kg/cm ² /m (Kilograms Per Square Cm Per Meter of Bed)	= 4.33 psi/ft = 1.03 atmos/m = 10 ft H ₂ O/ft

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PRSM is a free program that models all aspects of plant design associated with ion exchange resin performance and operation.



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